Removal of lead (II) ion from industrial wastewater by activated carbon prepared from *Vitex negundo* using batch adsorption studies

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The potential of chemically carbonized *Vitex negundo* stem (VNC) for the effective removal of lead (II) ion from aqueous solutions has been investigated in batch experiments. The activated carbon prepared from VNC has been modified using the activating agent H_2SO_4. Lead adsorption significantly depends on the initial concentration of lead (II), *p*H, adsorbent dosage, particle size, and the effect of temperature. FT-IR used to characterize the functional groups and the powder XRD data elaborated on the active sites predicted in VNC-1. The main structures of activated carbons are amorphous, as expected and predicted. The results indicate that the carbon prepared from VNC-1 activated could be used to effectively adsorb lead (II) ion from aqueous solutions. Further, the optimum conditions for adsorption studies are calculated, and it is concluded that the activated carbon exhibits a good adsorption potential for lead ions.

Keywords: Adsorption, Batch studies, FT-IR, Lead (II) ions, SEM, XRD

Lead in the natural environment arises from both natural and anthropogenic sources, and is detrimental to human health and all living things[1]. All lead compounds are considered cumulative poisons. Recently, increasing inters thus been focused on removing Pb(II) ions from drinking water due to its supreme toxicity to our health[2]. Drinking water contaminated with Pb(II) ions for long term, even if in a very low concentration, could lead to a wide spectrum of health problems, such as nausea, convulsions, coma, renal failure, cancer and subtle effects on metabolism and intelligence[3,4]. The maximum allowable lead concentration in drinking water has been set at 15 ppb by the US Environmental Protection Agency. A number of methods have been examined for the removal of lead from water, such as precipitation, coagulation, adsorption, ultra filtration, reverse osmosis, and membrane separation[5-7]. Among them adsorption is recognized as an effective and economic method for heavy metals removal[8, 9].

The presence of these heavy metals in streams and surface waters has been responsible for several health problems with animals, plants and human beings. Lead is a pollutant that is present in drinking water and in air. It is derived from lead emissions from automobiles because it is used as an anti knocking agent in the form of lead tetraethyl in gasoline. In water, lead is released in effluent from lead treatment and recovery industries, especially from lead battery manufacturing units[10]. Lead plays a major role in the manufacturing of cable sheathing, lining for chemical baths and storage vessels batteries, circuit boards, lining for chemical baths and storage vessels, chemical transmission pipes, electrical components and radiation shielding[11]. Lead continues to use extensively in rolled and extruded products in the construction industry. The use of lead sheeting in the building industry has increased in recent years[12]. Lead also has a variety of other uses, including the manufacture of water repellents, dyes, varnishes and resins, pigments, automotive parts, explosives, paper coatings, crystal vessels, ammunition, ceramic glazes, jewellery, toys, ceramics glass industries, rubber, plastics and in analytical applications[13]. Adsorption is a purely a surface phenomenon and mass transfer process by which it transfers ions from the liquid phase to the surface of a solid and becomes bound by physical and chemical interactions[14]. Various

functional groups like alcohol, aldehydes, ketones, carboxylic, ether, phenolic make these adsorbents effective towards metal binding and make the material as attractive for removing of heavy metals[15].

In the present work, the *Vitex negundo* stem was used as an adsorbent for the removal of Pb(II) ions from aqueous solutions. Our adsorption studies included the effects of pH, contact time, effect of temperature on the adsorption efficiency were studied. The chemical activation consists of more advantages compared to physical activation. H_2SO_4 helps to develop the porosity of carbon and improves the pore development of carbon structure and increases the yield of the carbon[16].

Experimental Section

The Sample of *Vitex negundo* stem was collected from an agricultural waste in Ariyalur district, Eravangudi village, Tamil Nadu, India. The procedure of preparation of material was followed as that reported. The stock solution of Pd(II) 1g/L was prepared from Pb(II),$8H_2O$. By using this stock solution the desired dilutions were made and used throughout the study[17].

The developed adsorbent was characterized as discussed.

Characterization of adsorbents

The order to characterize the surface structure of activated charcoal HR-SEM in F E I Quanta FEG 200 ZEISS analysis was carried out. The surface morphology involved in metal adsorption, XRD was performed on X'Pert-Pro, PAN analytical diffractometer operated at 30 kV/30 mA, to determine the material using CuKa1 radiation with wavelength of 1.54 A° in the wide angle region from 10^0 to 80^0 on 2θ scale. VNC-1 and lead (II) loaded/VNC-1. The functional group were analyzed using FT-IR spectra of the samples were recorded in the range of 400–4000 cm^{-1} Shimadzu spectrometer.

Results and Discussion

SEM

The surface texture and morphology of VNC-1 and VNC (1) / lead (II) was determined using scanning electron micro-graph. The availability of pores and internal surface, which is a requisite for a potential adsorbent, is clearly displayed in the SEM and EDAX picture of the before adsorption of VNC-1 and after adsorption of VNC (1)/lead (II) (Fig.1). The coverage of the surface and the pores by the adsorbed Pb(II) ions is displayed before characteristics work.

Spectral studies

The functional groups present in the active sites of an adsorbent are examined using FTIR spectroscopy. The functional groups present in the surface of the adsorbent are attributable for attracting the metal ion present in the solution. The functional groups present in VNC-1 and lead (II) loaded/ VNC-1 are shown in Fig. 2. The figure illustrates that peaks obtained in the range of 3340cm^{-1} reveals the acidic hydroxyl group present in the surface and the peaks at 3340-2920 cm^{-1} shows the presence of O-H groups present in the adsorbent. The peaks observed at 2919-2686 cm^{-1} indicates the presence of –CH and –CO groups and the peaks obtained at 1589-1585 cm^{-1} shows the presence of the N-H group as primary amines and –C-C group. The peaks at 1382-1353 cm^{-1} indicates the presence of CH groups on the surface of the VNC-1. The -C-Cl groups of alkyl halide present
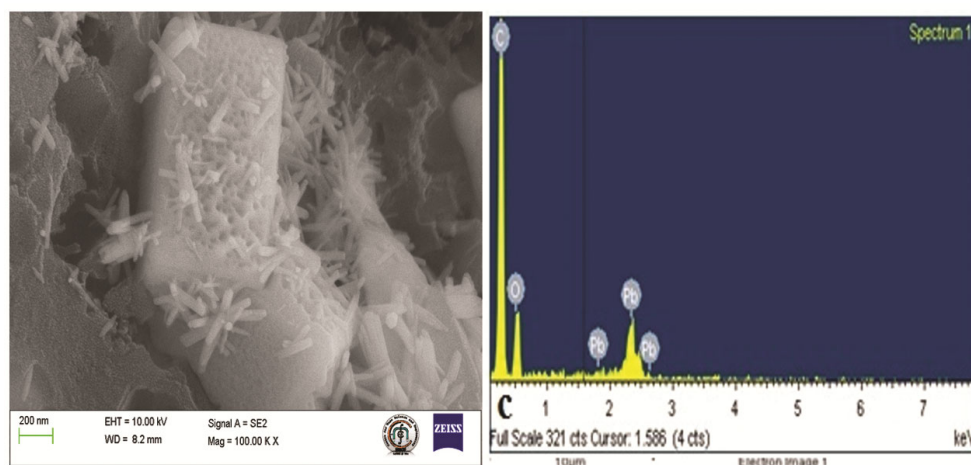

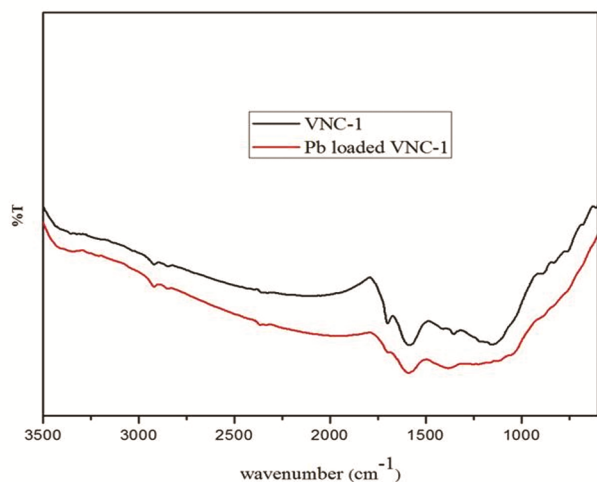Fig. 1 — SEM and EDX IMAGE OF VNC-1 after Pb(II) adsorption

Fig. 2 — FTIR spectrum of VNC-1 and Pb(II) loaded/ VNC-1

in the range of peaks obtained from 850-550 cm⁻¹. The adsorbents loaded with Pb(II) shows a similar FTIR spectrum as that obtained with an unloaded adsorbent, except that the bands had shifted to higher or lower values as shown in figure. The shifting of band due to the Pb(II) adsorption. Thus, the FTIR analysis revealed that the functional group like –OH, C-H bending, and C=O, COO-, O-H groups were mainly responsible for the adsorption.

X-Ray Diffraction (XRD)

X-ray diffraction (XRD) patterns of the powders were recorded at room temperature. The XRD pattern has a highly porous structure with sharp edges $2\theta = 25.48^0$ was appeared in VNC-1 after adsorption lead in VNC-1 the peak appeared prepared carbon gets slight diminished which shows an evidence of adsorption of metal ion. The powder XRD data active sites and 2θ as well as the d values present in VNC-1 and lead (II) loaded VNC-1 carbons are shown in Fig. 3.

Batch adsorption studies

Batch adsorption equilibrium experiments were conducted for the adsorption of lead on activated carbon of VNC-1 as a function of pH, initial Pb(II) concentration, adsorbent dose and contact time by adding 0.2 g of dried carbon to 100 mL of lead solution with different concentrations in 250 mL stoppered reagent bottles at a constant shaking. All the experiments were carried out at room temperature $30 \pm 1°C$. For studying the influence of pH on the adsorption of Pb(II), the experiments were conducted at various initial metal solution pH values of 3 to 7.
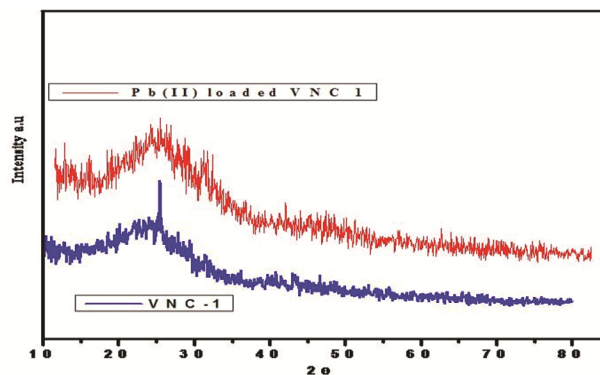

Fig. 3—XRD pattern of VNC-1 and Pb(II) loaded/ VNC-1

The pH of each solution was adjusted to different values with either 0.1 N NaOH or 0.1N HCL. All experiments were carried out by adding 50 mL of metal solution and adsorbent in an Erlenmeyer flask and made for constant stirring for 210 min. At the end of each experiment, the solution was filtered and the filtrate was titrated with EDTA solution during the adsorption, a rapid equilibrium established between adsorbed metal ions on the active cites of adsorbent (q_e) and unadsorbed metal ion in the solution. The amount of adsorption at equilibrium (q_e) (mg/g) and the percentage adsorption (%) were computed as Follows:

$$\text{Adsorption capacity } (q_e)\ (mg/g) = \frac{(C_o - C_e)\ V}{X}$$

$$\% \text{ Percentage Adsorptiom} \frac{C_o - C_e}{C_o} \times 100$$

where C_0 and C_e represented the initial and equilibrium concentrations (mg/L),
V - is the volume of solution and
X - is the weight of adsorbent (g).

Effect of initial Pb(II) concentration

The adsorption process on effect of initial concentration (100-500 mg/L) on the percent removal of Pb(II) is shown in Fig. 4(a). The result reveals as the increase in concentration of metal ion found to be a decrement in percent adsorption of Pb(II). The number of lead ions available at lower concentration of the solution is found to less as compared to the available sites on the adsorbent. However, at higher concentrations, the metal ions are greater than the available adsorption sites are saturated and thus, the percentage removal of lead ions depends on the initial concentration. The maximum percentage removal (80.00%) of Pb(II) was achieved at 100 mg/L of lead solution[18,19]. Comparison of VNC-1 Pb(II) with
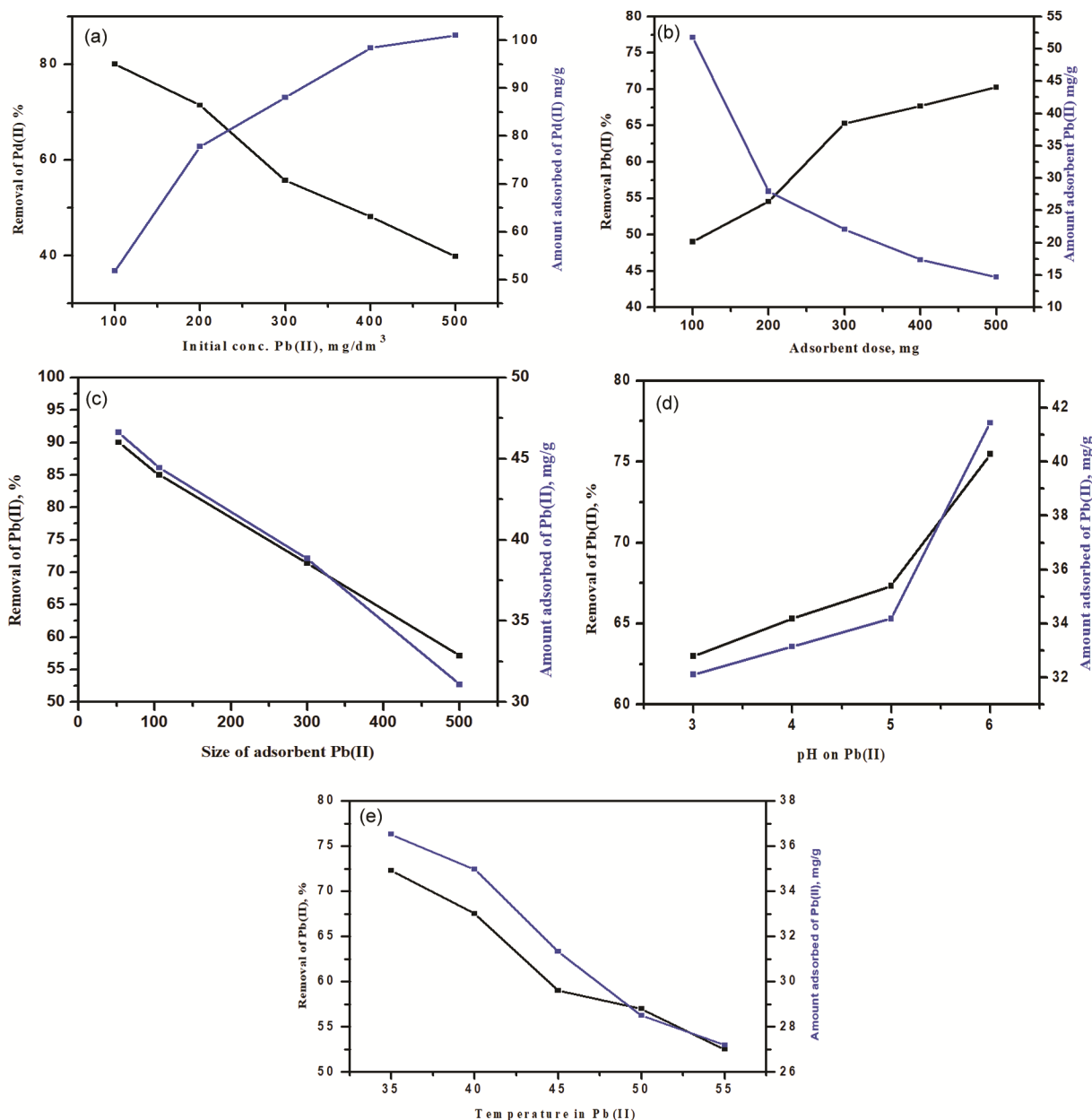
Fig. 4 ─ (a) Effect of initial concentration of adsorbent on removal of Pb(II) from aqueous solution Conditions: adsorbent dose=200mg; Size of adsorbent= 0-53μ;*p*H = 6; temperature = 30 ± 1°C; (b) Effect on dose of adsorbent on removal of Pb(II) from aqueous solution Conditions: Pb(II)=100mg/L; Size of adsorbent= 0-53μ;pH=6;Temperature = 30 ± 1°C; (c) Effect of Size of adsorbent on removal of Pb(II) from aqueous solution Conditions: Pb(II)=100mg/L; adsorbent dose=200mg; *p*H= 6; Temperature = 30 ± 1°C; (d) Effect of *p*H on removal of Pb(II) from aqueous solution Conditions: Pb(II)=100mg/L; adsorbent dose=200mg; Size of adsorbent= 0-53μ; Temperature= 30 ± 1°C and (e)Effect of temperature on removal of Pb(II) from aqueous solution Conditions: Pb(II)=100mg/L; adsorbent dose=200mg; Size of adsorbent= 0-53μ; *p*H=6

conventional adsorbents using the maximum adsorption capacity (Table 1).

Effect of adsorbent dosage

The adsorbent dose is another important parameter that influences the adsorption of metal ions onto the VNC-1. The experiments were carried out under the conditions by varying the adsorbent dosage from 100mg to 500mg. It will be seen that the removal efficiency towards Pb(II) ions increased as the adsorbent dosage increased is presented in Fig. 4 (b). The factor is that adsorption sites remain unsaturated during the adsorption reaction. This is due to the dosage of the adsorbent increased there is a less

Table 1 — Comparison of VNC-1 Pb(II) with conventional adsorbents using the maximum adsorption capacity (q max – mg/g).

No	Adsorbent	q_{max}(mg/g) amount adsorbed	References
1	Cork oak	187.28	(20)
2	Rattan	149.25	(21)
3	CAC	165.50	(22)
4	P.paluta sawdust	151	(23)
5	Rose petals waste	119.92	(24)
6	Onion skins	200.00	(25)
7	Orange peel	209.8	(26)
8	Orange peel	476.1	(27)
9	VNC-1	101.00	(38)

Table 2 — Optimum pH values in various Plant and VNC-1 Pb(II) adsorption systems

No	Adsorbent	Optimum pH	References
1	Portulaca plant biomass	6.0	(33)
2	Pineapple Peel fibre	5.6	(34)
3	Watermelon rind	6.8	(35)
4	Cocoa pod husk	6.0	(36)
5	Onion skins	6.0	(25)
6	Potato Peels	6.0	(37)
7	VNC-1	6.0	(38)

proportionate increase in adsorption resulting from the lower adsorptive capacity utilization of the adsorbent. As adsorbent dose increases, there will be a more and more surface area available which increases active sites for binding of metal ions and thus exchanges sites[28].

Effect of particle size on Pb (II) removal

Adsorption is a process of surface controlled phenomenon. The percentage removal of Pb(II) decreased with increasing adsorbent particle size as shown in Fig. 4 (c). The higher adsorption occurred in smaller adsorbent particle size is attributed due to the smaller particles give large surface areas offers a comparatively larger and more accessible surface area and hence, there was an increase of adsorption found as the size of the particle gets decreased. Thus, the adsorption equilibrium of lead found to be (90.00%) at180 min with size 0-53μ and increasing the adsorbent particle size to 53-106μ and 106-300μ and 300 -500μ leads to decrease of percent removal by (57.17%). For optimum condition, low particle size (53μ) was used for further experiments.

Effect of solution *p*H

The *p*H of the solution has a significant impact on the uptake of heavy metals, since it determines the surface charge of the adsorbent, the degree of ionization and speciation of the adsorbate. The optimum *p*H for the removal of Pb(II) from the solution with initial lead concentration of 100 mg/L was observed that the percent removal of Pb(II) found to be increased with increasing pH 3 to 6 further increment of *p*H = 7 cause decline in adsorption displayed in Fig. 4 (d). This is because at low *p*H, the active sites get protonated and thus the protonated H$^+$ ion competes with Pb(II) ions for the adsorption reaching the binding sites of the adsorbent caused by the repulsive forces. At high *p*H, the concentration of H$^+$ decreases hence they do not involve in metal ion on adsorption sites. The surface of the adsorbent with negative charge attracts positive charge of the metal ion easily towards its binding sites. At *p*H = 7, a decrease of adsorption of Pb(II) was observed due to the formation of lead hydroxide(29). The presence of Hydroxide species lowers the adsorption process onto adsorbent. Hence, the further experiments were conducted at optimal *p*H = 6. (30- 32). Optimum *p*H values in various Plant and VNC-1 Pb(II) adsorption systems (Table 2).

Effect of temperature

The effect of temperature on the removal of metal ions using VNC-1 was investigated at different temperatures (35°–55°C). On increasing temperature, the removal efficiency of metal ion decreased as the solution temperature was increasing from 35°C to 55vC as shown in Fig. 4 (e). The decrease in percentage may be due to desorption caused by an increase in the available thermal energy. At the high temperature higher mobility of the adsorbate is induced causing desorbed. This result shows that the nature of the adsorption processes is mainly due to the decrease in surface activity, suggesting that adsorption between Pb(II) and VNC-1is an exothermic process[35,36]. The maximum adsorption of metal ions by the VNC-1was obtained at 35°C which shows that the adsorption of metal ions onto the VNC-1 is highly dependent on the temperature observed a similar result. Therefore, the optimum temperature at 30±1°C used for further experiments[37-39].

Conclusion

In this study, the use of activated carbon prepared from chemically modified VNC-1 as adsorbents for removal of Pb(II)ions from aqueous solution. The batch study parameters, P^H of solution, initial Pb(II) concentration, adsorbent ,particle size, dose have been found to be effective on the adsorption. The maximum equilibrium has been achieved practically in 180 min. Further increment there is no significant

increase in adsorption. The FTIR analysis of VNC-1showed that different functional groups are involved in the adsorption of the Pb(II) ions and There is no appearance of any new functional group after adsorption of lead prove to adsorption occur through physically. The results may be very useful for designing an Economically cheap treatment process for the removal of Pb(II) containing waste water from Chemical industries. Based on the results of this research, VNC-1 can be considered as an Effective, available and natural adsorbent for removing Pb(II) from aqueous solutions.

Acknowledgements

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