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# Influences of Cattaneo-Christov Heat Flux, Joule Heating, Viscous Dissipation and Chemical Reaction on Hydromagnetic Pulsating Flow of Oldroyd-B Nanofluid in a Porous Channel

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In this present study, Cattaneo-Christov heat flux on the hydromagnetic pulsatile flow of Oldroyd-B nanofluid through a porous channel with the presence of Brownian motion, thermal radiation, and thermophoresis effects are studied. The effects of dissipation of viscous and Ohmic heating are considered. The Buongiorno model is taken into account in this analysis. By using the perturbation method the governing partial differential equations (PDEs) are converted into the ordinary differential equations (ODEs) and solved numerically by employing the Runge-Kutta 4<sup>th</sup>-order scheme along with shooting approach. The influence of distinct parameters on velocity, temperature, nanoparticle concentration, heat and mass transfer rates are examined in detail. The results indicate that nanofluid velocity increases with higher frequency parameter, and while it falls with rising Hartmann number, and cross-flow Reynolds number. An increase in thermophoresis parameter, Eckert number, radiation parameter, Brownian motion parameter leads to a rise in temperature whereas temperature decreases for increasing Hartmann number and thermal relaxation time parameter. Moreover, the nanoparticle concentration enhances with an increasing thermophoresis parameter, thermal relaxation time parameter while it falls with the rising values of Lewis number, chemical reaction parameter and Brownian motion parameter.

Keywords: Pulsatile flow; Oldroyd-B nanoliquid; Cattaneo-Christov heat flux; Joule heating; chemical reaction; Brownian motion; thermophoresis

## **1** Introduction

The study of pulsatile flow has gotten a lot of attention of researchers because of its implementations in engineering and science, such the reciprocal pumps, respiratory system, as microelectromechanical system, vascular diseases, IC engines, and circulatory system<sup>1-7</sup>. Srinivas et al.<sup>8</sup> deliberated the influence of thermal diffusion, thermal radiation, and chemical reaction on the hydromagnetic pulsatile flow of non-Newtonian fluid in a channel. governing flow equations were The solved analytically by using the perturbation technique. Bilgi and Atalik<sup>9</sup> numerically explored the elastic properties of blood in terms of their effects on pulsatile arterial hemodynamics, such as the vorticity, velocity, stress fields, and indicators of aneurysm rupture. Ponalagusamy and Manchi<sup>10</sup> discussed the combined effects of magnetic and electrical fields on the pulsating flow of Jeffery fluid with particles suspended in stenosed arteries. Kumar and Srinivas<sup>11</sup> researched the pulsating flow of MHD blood $Al_2O_3/Cu/Ag/Au$  nanofluid in a vertical porous channel with velocity slip and Joule's heating impacts at the walls. Recently, Venkatesan and Reddy<sup>12</sup> analytically explored the hydromagnetic pulsatile flow of Au/CuO-blood non-Newtonian nanoliquid through a porous channel with Joule heating, dissipation of viscous, applied magnetic field, and thermal radiation effects.

The term nanofluid generally refers to the suspension of rigid nanometer-sized (1-100 nm) particles in a liquid. Choi<sup>13</sup> first proposed the development of nanofluid in 1995. Nanofluid is critically important in the modern world because of its wide array of applications in biomedicine, energy storage, cancer therapy, industrial cooling, nano-drug delivery, and electromechanical system<sup>14-21</sup>. Buongiorno<sup>22</sup> inspected the convective heat transfer in a nanoliquid. A two-component, non-homogeneous 4equation equilibrium model for nanoliquid was developed by the author. Xu et al.23 derived a mathematical model for the Buongiorno mixed convection flow of a nanofluid in a vertical channel by using the homotopy analysis method (HAM). Zheng et al.<sup>24</sup> studied the radiation heat transfer of a

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nanofluid over a stretching sheet by using local similarity method. Srinivas et al.<sup>25</sup> intended the hydromagnetic flow of a nanoliquid through a porous channel along with slowly growing or shrinking walls by utilizing HAM. Kumar et al.<sup>26</sup> used the Buongiorno nanofluid model to analyse the hydromagnetic pulsating flow of non-Newtonian nanoliquid in a vertical channel inserted in a porous medium along with the presence of heat absorption *et* al.<sup>27</sup> and thermal radiation. Abdelmalek numerically examined impacts of thermophoretic diffusion and Brownian motion on electrically conducting nanofluid by employing R-K-Fehlberg method. Xu et al.<sup>28</sup> theoretically deliberated the applications of activation energy, induced magnetic force, and non-uniform heat sink/source on third grade nanofluid. Recently, Rajamani and Reddy<sup>29</sup> analytically studied the MHD pulsating flow of blood-Al<sub>2</sub>O<sub>3</sub> non-Newtonian nanofluid through a channel based on the viscous dissipation and Ohmic heating effects by applying the perturbation method.

Many substances, such as lubricants, blood, ketchup, paints, dyes, ice creams, toothpaste, vaccines, cosmetics, syrups, and specific care products are non-Newtonian fluid, these do not obey the Newtonian manner. The non-Newtonian fluid model has been received much interest of several researchers<sup>30-36</sup>. Oldroyd-B fluid model is one of viscoelastic non-Newtonian fluid model. Malathy et al.<sup>37</sup> analytically explored the MHD pulsatile flow of an Oldroyd-B fluid with chemical reaction and radiation effects in a porous medium with convective and slip boundary conditions. Kumaran and Sandeep<sup>38</sup> theoretically inspected MHD non-Newtonian fluids towards a high revolutionary paraboloid with Brownian moment and numerically solved the governing equation by utilizing Runge-Kutta 4<sup>th</sup>-order scheme along with shooting technique. Javid et al.<sup>39</sup> evaluated the viscosity characteristics of non-Newtonian fluid with synthesized Fe<sub>3</sub>O<sub>4</sub> added to glycerine, engine oil, paraffin oil, and distilled water for application in thermal system. Khan et al.40 numerically researched the 2D steady non-Newtonian fluid flow and the heat transfer around a heated square cavity with a Y-shaped fin under the effects of thermal radiation and magnetic field by employing the Galerkin weighted residual technique of the finite element method. Recently, Venkatesan and Reddy<sup>41</sup> inspected the effects of the pulsating flow of bloodalumina Oldroyd-B (non-Newtonian) nanoliquid in a channel with Ohmic heating, dissipation of viscous,

and magnetic field impacts by utilizing the perturbation method.

Heat transfer has a wide range of uses in current technology, including cooling nuclear reactors, magnetic drug targeting, medicinal application, and cooling of energy-producing areas, among others. The fundamental Fourier<sup>42</sup> law is one of the most wellknown laws in classical physics for explaining the heat transfer process in a variety of situations. One of the fundamental flaws of the parabolic equation for heat is that is it causes disruption while also challenging the concept of determinism over the entire medium. Cattaneo<sup>43</sup> broke over this barrier by interlacing relaxation time with heat flux. Cattaneo's proposed model was improved by Christov<sup>44</sup>, who included Oldroyd's upper convected derivatives. His adaptation is known as the Cattaneo-Christov heat flux model. Haddad<sup>45</sup> studied thermal instability in a Brinkman porous media with fluid inertia. There is research into both fixed-fixed and free-free boundaries. The Cattaneo-Christov theory has been incorporated into the constitutive heat flux equation. Ibrahim et al.<sup>46</sup> examined the impacts of Cattaneo-Christov heat and mass diffusions on viscoelastic nanofluid with 3<sup>rd</sup> order slip flow condition. Shah et al.47 discussed non-isothermal micropolar fluid flow over a nonlinearly extending surface using Cattaneo-Christov heat flux model. Chu et al.48 investigated the thermal and solutal relaxation characteristics of the prediction methodology of double diffusions Cattaneo-Christov on 2D magnetohydrodynamics boundary layer flow of second-grade nanofluid.

The survey bespeak that no attempt has yet been made to inspect Cattaneo-Christov heat flux model on the pulsating flow of Oldroyd-B nanoliquid through a porous channel with Brownian motion, chemical reaction, thermophoresis, Joule heating, and viscous dissipation effects. Based on previous studies, we made an attempt to examine the effects of chemical reactions, thermophoresis, Brownian motion, viscous dissipation, and Joule heating with Cattaneo-Christov heat flux model on the pulsatile hydromagnetic flow of Oldroyd-B within a porous channel. By using the perturbation method, the governing PDEs are reduced to ODEs and then numerically resolved by employing Runge-Kutta 4<sup>th</sup>-order scheme along with shooting method. The velocity, temperature, and nanoparticle concentration of nanofluid are discussed in detail with using pictorial results by varying various emerging parameters. The heat transfer rate and mass transfer rate are deliberate using tables in detail for various parameters.

## **2** Formulation of the problem

Consider the incompressible and laminar hydromagnetic pulsating flow of Oldroyd-B nanofluid in a porous channel in the presence of Cattaneo-Christov heat flux. Joule heating, viscous dissipation, chemical reaction implication are taken into account. The Brownian motion and thermophoresis effects are analysing by using the Buongiorno nanofluid model. As shown in Fig. 1 Cartesian coordinate system is taken such that the  $x^*$ -axis is along to the bottom wall, and the  $y^*$ -axis is perpendicular to the walls. Fluid injected with velocity  $v_0$  through the bottom wall and suctioned out through the top wall at the same rate. The walls are separated by the distance h. A strength of the magnetic field  $B_0$  is consistently applied orthogonally to the walls.  $T_0$  and  $C_0$  are the temperature and nanoparticle concentration of bottom walls respectively.  $T_1(>T_0)$  and  $C_1(>C_0)$  are the temperature and nanoparticle concentration of top walls respectively. Assume that the pulsating flow is driven by an unsteady pressure gradient of the form<sup>2</sup>, 3, 9, 26

$$-\frac{1}{\rho_f}\frac{\partial P^*}{\partial x^*} = A(1 + \varepsilon e^{i\omega t^*}), \qquad \dots (1)$$

where  $\mathcal{O}$  is frequency,  $\varepsilon(<<1)$  is a positive quantity, A is a constant,  $t^*$  is dimensional time,  $\rho_f$  is the density of the fluid. The current examination is constructed from the Oldroyd-B model on the



Fig. 1 — Flow geometry.

viscoelastic fluid model. According to the aforementioned assumptions, the governing flow equations are

$$\begin{pmatrix} 1 + \lambda_1 \frac{\partial}{\partial t^*} \end{pmatrix} \frac{\partial u^*}{\partial t^*} + v_0 \begin{pmatrix} 1 + \lambda_1 \frac{\partial}{\partial t^*} \end{pmatrix} \frac{\partial u^*}{\partial y^*} \\ = -\frac{1}{\rho_f} \begin{pmatrix} 1 + \lambda_1 \frac{\partial}{\partial t^*} \end{pmatrix} \frac{\partial P^*}{\partial x^*} + \frac{\mu_f}{\rho_f} \begin{pmatrix} 1 + \lambda_2 \frac{\partial}{\partial t^*} \end{pmatrix} \frac{\partial^2 u^*}{\partial y^{*2}} \\ -\frac{\sigma_f}{\rho_f} \begin{pmatrix} 1 + \lambda_1 \frac{\partial}{\partial t^*} \end{pmatrix} B_0^2 u^*, \qquad \dots (2)$$

$$\frac{\partial T^{*}}{\partial t^{*}} + v_{0} \frac{\partial T^{*}}{\partial y^{*}} + \lambda_{3} \left( \frac{\partial^{2} T^{*}}{\partial t^{*2}} + v_{0}^{2} \frac{\partial^{2} T^{*}}{\partial y^{*2}} \right)$$

$$+ 2v_{0} \frac{\partial^{2} T^{*}}{\partial y^{*} \partial t^{*}} = \frac{k_{f}}{\left(\rho C_{p}\right)_{f}} \frac{\partial^{2} T^{*}}{\partial y^{*2}} - \frac{1}{\left(\rho C_{p}\right)_{f}} \frac{\partial q_{r}}{\partial y^{*}}$$

$$+ \frac{\mu_{f}}{\left(\rho C_{p}\right)_{f}} \left( \frac{\partial u^{*}}{\partial y^{*}} \right)^{2} + \frac{\sigma_{f}}{\left(\rho C_{p}\right)_{f}} B_{0}^{2} u^{*2}$$

$$+ \tau_{1} \left[ D_{B} \left( \frac{\partial T^{*}}{\partial y^{*}} \frac{\partial C^{*}}{\partial y^{*}} \right) + \frac{D_{T}}{T_{m}} \left( \frac{\partial T^{*}}{\partial y^{*}} \right)^{2} \right], \qquad \dots (3)$$

$$\frac{\partial C^{*}}{\partial t^{*}} + v_{0} \frac{\partial C^{*}}{\partial y^{*}} = D_{B} \frac{\partial^{2} C^{*}}{\partial y^{*2}} + \frac{D_{T}}{T_{m}} \frac{\partial^{2} T^{*}}{\partial y^{*2}} - k_{r} C^{*},$$

$$\dots (4)$$

here,  $u^*$  is the dimensional velocity on  $x^*$  direction,  $T^*$  and  $C^*$  are the dimensional temperature and dimensional concentration of the fluid,  $P^*$  is the pressure,  $v_f$  is the kinematic viscosity of the fluid,  $\sigma_{_{f}}$  is the electrical conductivity of the fluid,  $\lambda_{_{1}}$  and  $\lambda_2$  are relaxation and retardation times respectively,  $k_{f}$  is the thermal conductivity of the fluid,  $\mu_{f}$ is the dynamic viscosity of the fluid,  $(\rho C_P)_f$ is the effective heat capacity of fluid,  $\lambda_3$  is the relaxation time of heat flux,  $D_B$  is Brownian diffusion coefficient,  $D_r$  is the thermophoretic diffusion coefficient. is temperature,  $T_m$ mean  $\tau_1 = (\rho C_P)_p / (\rho C_P)_f$ ,  $(\rho C_P)_p$  is the effective heat capacity of the nanoparticles and  $k_r$  is the firstorder chemical reaction rate.

The corresponding boundary conditions (B.Cs) are as follows:

$$u^{*}(0) = 0, T^{*}(0) = T_{0}, C^{*}(0) = C_{0}, \dots$$
 (5)

$$u^{*}(h) = 0, T^{*}(h) = T_{1}, C^{*}(h) = C_{1}.$$
 ... (6)

Now, with the use of Rosseland approximation for radiative heat flux,  $q_r$  and by following <sup>24, 37</sup> Eqn. (3) becomes

$$\frac{\partial T^{*}}{\partial t^{*}} + v_{0} \frac{\partial T^{*}}{\partial y^{*}} + \lambda_{3} \left( \frac{\partial^{2} T^{*}}{\partial t^{*2}} + v_{0}^{2} \frac{\partial^{2} T^{*}}{\partial y^{*2}} \right)$$

$$+ 2v_{0} \frac{\partial^{2} T^{*}}{\partial y^{*} \partial t^{*}} = \frac{k_{f}}{\left(\rho C_{p}\right)_{f}} \frac{\partial^{2} T^{*}}{\partial y^{*2}} + \frac{\mu_{f}}{\left(\rho C_{p}\right)_{f}} \left( \frac{\partial u^{*}}{\partial y^{*}} \right)^{2}$$

$$+ \frac{\sigma_{f}}{\left(\rho C_{p}\right)_{f}} B_{0}^{2} u^{*2} + \frac{1}{\left(\rho C_{p}\right)_{f}} \frac{16T_{1}^{3}\hat{\sigma}}{3\xi} \frac{\partial^{2} T^{*}}{\partial y^{*2}}$$

$$+ \tau_{1} \left[ D_{B} \left( \frac{\partial T^{*}}{\partial y^{*}} \frac{\partial C^{*}}{\partial y^{*}} \right) + \frac{D_{T}}{T_{m}} \left( \frac{\partial T^{*}}{\partial y^{*}} \right)^{2} \right], \qquad \dots (7)$$

here,  $\xi$  is the Rosseland mean absorption coefficient and  $\hat{\sigma}$  is the Stefan-Boltzmann constant.

Now, by using the following non-dimensional parameters and variables,

$$x = \frac{x^{*}}{h}, y = \frac{y^{*}}{h}, P = \frac{P^{*}}{\rho_{f}Ah}, u = \frac{\omega u^{*}}{A},$$
  
$$t = t^{*}\omega, \theta = \frac{T^{*} - T_{0}}{T_{1} - T_{0}}, \phi = \frac{C^{*} - C_{0}}{C_{1} - C_{0}}$$
  
$$(8)$$

Eqns. (1), (2), (7), and (4) become

$$-\frac{\partial P}{\partial x} = 1 + \varepsilon e^{it}. \qquad \dots (9)$$

$$H^{2} \left( 1 + \lambda_{1} \omega \frac{\partial}{\partial t} \right) \frac{\partial u}{\partial t} + R \left( 1 + \lambda_{1} \omega \frac{\partial}{\partial t} \right) \frac{\partial u}{\partial y}$$

$$= -H^{2} \left( 1 + \lambda_{1} \omega \frac{\partial}{\partial t} \right) \frac{\partial P}{\partial x} + \left( 1 + \lambda_{2} \omega \frac{\partial}{\partial t} \right) \frac{\partial^{2} u}{\partial y^{2}}$$

$$-M^{2} \left( 1 + \lambda_{1} \omega \frac{\partial}{\partial t} \right) u, \qquad \dots (10)$$

$$H^{2} \frac{\partial \theta}{\partial t} + R \frac{\partial \theta}{\partial y} + \delta \left[ H^{2} \frac{\partial^{2} \theta}{\partial t^{2}} + \frac{R^{2}}{H^{2}} \frac{\partial^{2} \theta}{\partial y^{2}} \right]$$

$$+2R\frac{\partial^{2}\theta}{\partial y\partial t}\bigg] = \frac{1}{\Pr}\bigg(1+\frac{4}{3}Rd\bigg)\frac{\partial^{2}\theta}{\partial y^{2}} + Ec\bigg(\frac{\partial u}{\partial y}\bigg)^{2}$$
$$+EcM^{2}u^{2} + Nb\frac{\partial\theta}{\partial y}\frac{\partial\phi}{\partial y} + Nt\bigg(\frac{\partial\theta}{\partial y}\bigg)^{2}, \qquad \dots (11)$$
$$H^{2}\Pr Le\frac{\partial\phi}{\partial t} + R\Pr Le\frac{\partial\phi}{\partial y} = \frac{\partial^{2}\phi}{\partial y^{2}}$$

$$+\frac{Nt}{Nb}\frac{\partial^2\theta}{\partial y^2} - \gamma Le \operatorname{Pr} \phi - K_1 Le \operatorname{Pr}, \qquad \dots (12)$$

where,  $H = h \sqrt{\frac{\omega}{v_f}}$  is frequency parameter,

 $R = \frac{v_0 h}{v_f} \text{ is cross-flow Reynolds number, } \alpha = \frac{k_f}{(\rho C_p)_f}$ is thermal diffusivity,  $\delta = \omega \lambda_3$  is thermal relaxation time parameter,  $M = B_0 h \sqrt{\frac{\sigma_f}{\mu_f}}$  is Hartmann number,

$$Ec = \frac{A^2}{\omega^2 (C_P)_f (T_1 - T_0)} \text{ is Eckert number, } \Pr = \frac{v_f}{\alpha} \text{ is}$$
  
Prandtl number,  $Rd = \frac{4\hat{\sigma}T_1^3}{k_f \zeta}$  is radiation parameter,  
 $Nt = \frac{\tau_1 D_r (T_1 - T_0)}{T_m v_f}$  is thermophoresis parameter,  
 $Nb = \frac{\tau_1 D_B (C_1 - C_0)}{v_f}$  is Brownian motion parameter,  
 $\gamma = \frac{k_r h^2}{v_f}$  is chemical reaction parameter,  $Le = \frac{\alpha}{D_B}$  is  
Lewis number and  $K_1 = \frac{k_r C_0 h^2}{v_f (C_1 - C_0)}$ .

The corresponding B.Cs are

$$u(0) = 0, \quad \theta(0) = 0, \quad \phi(0) = 0, \quad \dots (13)$$
  
 $u(1) = 0, \quad \theta(1) = 1, \quad \phi(1) = 1. \quad \dots (14)$ 

#### **3 Method of Solution**

In consideration of Eq. (9), we assume the dimensionless velocity u, temperature  $\Theta$ , and nanoparticle concentration  $\phi$  are

$$u(y) = u_0(y) + \varepsilon e^{it} u_1(y),$$
  

$$\theta(y) = \theta_0(y) + \varepsilon e^{it} \theta_1(y),$$
  

$$\phi(y) = \phi_0(y) + \varepsilon e^{it} \phi_1(y)$$
  
...(15)

Now, by substituting Eqns. (9) and (15) into (10)-(12) and equating the terms like various powers of  $\mathcal{E}$ , one can get

$$\frac{d^2 u_0}{dy^2} - R \frac{d u_0}{dy} - M^2 u_0 + H^2 = 0, \qquad \dots (16)$$

$$\frac{d^{2}u_{1}}{dy^{2}} - R\beta^{2}\frac{du_{1}}{dy} - (M^{2} + iH^{2})\beta^{2}u_{1} + \beta^{2}H^{2} = 0,$$
... (17)

$$\left(1 + \frac{4}{3}Rd - \delta \operatorname{Pr}\frac{R^{2}}{H^{2}}\right)\frac{d^{2}\theta_{0}}{dy^{2}} - R\operatorname{Pr}\frac{d\theta_{0}}{dy}$$
$$+ \operatorname{Pr}Nb\frac{d\theta_{0}}{dy}\frac{d\phi_{0}}{dy} + \operatorname{Pr}Nt\left(\frac{d\theta_{0}}{dy}\right)^{2} + \operatorname{Pr}Ec\left(\frac{du_{0}}{dy}\right)^{2}$$
$$+ \operatorname{Pr}EcM^{2}u_{0}^{2} = 0, \qquad \dots(18)$$

$$\left(1 + \frac{4}{3}Rd - \delta \operatorname{Pr} \frac{R^{2}}{H^{2}}\right) \frac{d^{2}\theta_{1}}{dy^{2}} - i\operatorname{Pr} H^{2}\theta_{1}$$
$$-\operatorname{Pr} R\left(1 + 2i\delta\right) \frac{d\theta_{1}}{dy} + \operatorname{Pr} Nb\left(\frac{d\theta_{0}}{dy}\frac{d\phi_{1}}{dy} + \frac{d\theta_{1}}{dy}\frac{d\phi_{0}}{dy}\right)$$
$$+ 2\operatorname{Pr} Nt \frac{d\theta_{0}}{dy}\frac{d\theta_{1}}{dy} + 2\operatorname{Pr} Ec \frac{du_{0}}{dy}\frac{du_{1}}{dy}$$
$$+ 2\operatorname{Pr} EcM^{2}u_{0}u_{1} + \delta \operatorname{Pr} H^{2} = 0, \qquad \dots (19)$$

$$\frac{d^2\phi_0}{dy^2} - R \operatorname{Pr} Le \frac{d\phi_0}{dy} - \gamma Le \operatorname{Pr} \phi_0$$
  
+  $\frac{Nt}{Nb} \frac{d^2\theta_0}{dy^2} - K_1 Le \operatorname{Pr} = 0, \qquad \dots (20)$   
 $\frac{d^2\phi_1}{dy^2} - R \operatorname{Pr} Le \frac{d\phi_1}{dy} - (\gamma + iH^2) Le \operatorname{Pr} \phi_1$ 

$$+\frac{Nt}{Nb}\frac{d^2\theta_1}{dy^2} = 0, \qquad \dots (21)$$

where 
$$\beta^2 = \frac{1 + \lambda_1 i \omega}{1 + \lambda_2 i \omega}$$
.

The corresponding B.Cs are

$$\begin{array}{c} u_0(0) = 0, \ \theta_0(0) = 0, \ \phi_0(0) = 0, \\ u_1(0) = 0, \ \theta_1(0) = 0, \ \phi_1(0) = 0 \end{array} \right\}, \qquad \dots (22)$$

$$u_{0}(1) = 0, \ \theta_{0}(1) = 1, \ \phi_{0}(1) = 1, \\ u_{1}(1) = 0, \ \theta_{1}(1) = 0, \ \phi_{1}(1) = 0 \end{cases} \qquad \dots (23)$$

The physical quantities like heat and mass transfer rates (Nusselt and Sherwood numbers) in the dimensionless form at the walls are given as<sup>2</sup>

$$Nu = \left(\frac{d\theta_0}{dy} + \varepsilon \frac{d\theta_1}{dy} e^{it}\right)_{y=0,1}, \qquad \dots (24)$$

$$Sh = \left(\frac{d\phi_0}{dy} + \varepsilon \frac{d\phi_1}{dy} e^{it}\right)_{y=0,1}.$$
 (25)

Now, The system of Eqns. (16)-(21) with the B.Cs (22)-(23) are solved numerically by utilizing Ruge-Kutta fourth-order scheme using the shooting method. The step size is fixed as 0.001 ( $\Delta y = 0.001$ ).  $1 \times 10^{-10}$  correctness is fixed for the converging criteria.

To ensure the correctness of the current results, we compared them with the results obtained by NDSolve using the MATHEMATICA software, which are shown in Table 1. It can be seen that there is a good agreement between the results obtained by NDSolve and the current results.

Table 1 — Comparison between the present results and the results obtained by NDSolve for heat and mass transfer rates at the wall y = 0 for different values of *M*, and  $\delta$  when H = 2, R = 0, Ec = 0.5, Pr = 21, Rd = 1, Nb = 0.2, Nt = 0.2, Le = 2,

$K_1 = 0.001, \ \gamma = 1, \ \lambda_1 = 0.5, \ \lambda_2 = 0.8, \ \omega = 2, \ t = \pi / 3, \ \varepsilon = 0.001.$									
Parameters	values	$\theta'(y)$ at $y=0$		$\phi'(y)$ at $y=0$					
		NDSolve	Present result	NDSolve	Present result				
М	1	9.9790097	9.9790095	-5.751406	-5.751403				
	2	9.0977212	9.0977186	-5.020325	-5.020321				
	3	7.7060661	7.7060645	-3.990262	-3.990260				
δ	0.1	9.0977212	9.0977186	-5.020325	-5.020321				
	0.3	9.1012676	9.1012657	-5.022169	-5.022166				
	0.5	9.1048140	9.1048120	-5.024014	-5.024010				

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## 4 Result and discussion

The existing sector describes the influence of different values of several parameters on velocity, nanoparticle temperature, and concentration distribution which are given in Figs. 2-7. In this present analysis  $\mathcal{U}_s$ ,  $\theta_s$ , and  $\phi_s$  are represent steady velocity, steady temperature, and steady nanoparticle concentration respectively.  $u_t$ ,  $\theta_t$ , and  $\phi_t$  are represents unsteady velocity, unsteady temperature, and unsteady nanoparticle concentration of Oldroyd-B nanoliquid respectively. Throughout the analysis the parameters' values are taken as H = 2, M = 2, Ec = 0.5, Pr = 21, Rd = 1, Nb = 0.2, R = 1.



Fig. 2 — Steady velocity (a) influence of H = 1, 2, 2.5, (b) influence of M = 1, 2, 3, (c) influence of R = 1, 2, 3

Nt = 0.2, Le = 2,  $K_1 = 0.001$ ,  $\gamma = 1$ ,  $\lambda_1 = 0.5$ ,  $\lambda_2 = 0.8, \ \delta = 0.1, \ \omega = 2, \ t = \pi/3, \ \varepsilon = 0.001$ , unless otherwise stated. The steady velocity distribution of Oldroyd-B nanofluid for various values of frequency parameter (H), Hartmann number (M), and crossflow Reynolds number (R) are illustrated in Figs. 2(a-c). Fig. 2(a) indicates that greater frequency parameter increases the steady velocity  $u_{\rm s}$ . The reason is that an increase in frequency rises the velocity of the nanofluid. The steady velocity declines with increasing Hartmann number, as shown in Fig. 2(b). The purpose for the decrease in velocity is that the retarding forces which are created by the applied magnetic field are acted orthogonal to the flow direction and hence there is a decrease in the velocity. Fig. 2(c) shows that increasing *R* expedites steady velocity near the top wall while it retards near the bottom wall. The unsteady velocity distribution of Oldroyd-B nanofluid for various values of frequency parameter (H), Hartmann number (M), non-Newtonian parameters  $(\lambda_1, \lambda_2)$ , cross-flow Reynolds number (R), and time (t) are shown in Figs. 3(a-f). Fig. 3(a) describes the growth in H rises the unsteady velocity because a rise in frequency boosts up the velocity of the nanofluid. Fig. 3(b) illustrates increasing *M* causes decline in unsteady velocity. This decline is by reason of Lorentz's force generated by the applied magnetic field inside the system. The unsteady velocity is an increasing function of  $\lambda_1$  (see Fig. 3(c)). The opposite behavior is portrayed in Fig. 3(d) by the various values of  $\lambda_2$ . Fig. 3(e) represents  $u_i$  accelerate closer to the suction wall (top wall) while it falling closer to the injection wall (bottom wall) for increasing R. From Fig. 3f one can

notice that  $u_t$  is fluctuating for different values of t.

Figs. 4(a-f) illustrate the impacts of Eckert number (Ec), radiation parameter (Rd), thermal relaxation time parameter  $(\delta)$ , Hartmann number (M), Brownian motion parameter (Nb), and thermophoresis parameter (Nt) respectively on steady temperature  $\theta_s$  of nanoliquid. As seen in Fig. 4(a), increasing Ec rises the steady temperature of nanofluid. Ec is the relationship between the enthalpy and the kinetic energy. An increases in Ec leads to boost up the kinetic energy of particles by reducing enthalpy factor and that rises the temperature of the nanofluid.

effect of  $\theta_{s}$ is presented in he Rd on Fig. 4(b). It shows that larger Rd generates extra heat within the system, which will enhance thermal boundary layers. Therefore, rising Rd increases  $\theta_{a}$  of the nanofluid. From Fig. 4(c) one can depicts that rising  $\delta$  reduces the fluid temperature. The reason is that for higher values of thermal relaxation parameter  $\delta$  the particles of quantifiable material have a greater chance of supplying heat to their adjacent particles when the relaxation time parameter of heat flux is increased, thus the temperature reduces. According to Fig. 4(d), a higher Hartmann number declines the steady temperature of nanofluid. There is a possibility that Lorentz's force generated by an applied magnetic field converts to a resistive drag force, which would explain this decline. Fig. 4(e) portrays the influence of Nb on  $\Theta_s$ . It is clear that rising Nb substantially boosts the fluid temperature. The same nature, we can be seen in Fig. 4(f) by varying Nt.

The effects of M, Ec,  $\lambda_1$ ,  $\lambda_2$ , Rd and  $\delta$  on  $\Theta_t$ are demonstrated in Figs. 5(a-f) respectively. From these figures one can see that  $\Theta_t$  is wavering and the



Fig. 3 — Unsteady velocity (a) influence of H = 1, 2, 2.5, (b) influence of M = 1, 2, 3, (c) influence of  $\lambda_1 = 0.2, 0.5, 1$ , (d) influence of  $\lambda_2 = 0.2, 0.5, 1$ , (e) influence of R = 1, 2, 3, and (f) influence of  $t = \pi, \frac{3\pi}{4}, \frac{2\pi}{3}, \frac{\pi}{2}, \frac{\pi}{3}, 2\pi$ 



Fig. 4 — Steady temperature (a) influence of Ec = 0, 0.3, 0.5, (b) influence of Rd = 1, 2, 3, (c) influence of  $\delta = 0.1, 0.2, 0.3$ , (d) influence of M = 1, 2, 3, (e) influence of Nb = 0.1, 0.5, 1, (f) influence of Nt = 0.1, 0.2, 0.3

utmost is near the suction wall. Fig. 5(a) shows that escalating M wavering  $\Theta_t$ . Fig. 5(b) displays that up rise Ec escalates  $\Theta_t$ . The reason is that the heat generated by viscous dissipation may be responsible for this temperature escalates. The same action can be noted that in Fig. 5(c) by growing  $\lambda_1$ .  $\Theta_t$  is a decreasing function of  $\lambda_2$  (see Fig. 5(d)). Fig. 5(e) shows that  $\Theta_t$  is oscillating for higher Rd. Fig. 5(f), detected that  $\Theta_t$  rises for increasing  $\delta$ .

Figures. 6(a-e) demonstrate the impacts of chemical reaction ( $\gamma$ ), Lewis number (*Le*),

thermophoresis parameter (*Nt*), Brownian motion parameter (*Nb*), and thermal relaxation time parameter ( $\delta$ ) on nanoparticle concentration of nanofluid correspondingly. Fig. 6(a) discloses that  $\phi_s$ is reduced for a given rise in the chemical reaction parameter  $\gamma$ . The effect of *Le* on  $\phi_s$  is portrayed in Fig. 6(b). As one might expect that increasing Lewis number reduces  $\phi_s$ . This may be because an increase in Lewis number increases the rate of mass transfer and thus reduces the nanoparticles concentration. Fig. 6(c) reveals that  $\phi_s$  improves for a better estimate of *Nt*. The steady nanoparticle concentration



Fig. 5 — Unsteady temperature when H = 2.5 (a) influence of M = 1, 2, 3, (b) influence of Ec = 0, 0.5, 1, (c) influence of  $\lambda_1 = 0.2, 0.5, 1$ , (d) influence of  $\lambda_2 = 0.2, 0.5, 1$ , (e) influence of Rd = 1, 2, 3 and (f) influence of  $\delta = 0.1, 0.2, 0.3$ 

decreases as Nb increases because nanoparticles collide more rapidly and more heat is produced (see Fig. 6(d)). The contrary action can be seen in Fig. 6(e) for higher  $\delta$ .

Figures. 7(a-d) contrived the inspirations of Nb, Nt,  $\delta$  and t on  $\phi_r$ . Fig. 7(a) depicts that increasing Nb enhanced  $\phi_r$  near the walls while it falls near the middle of the channel. The opposite behavior is depicted in Figs. 7(b) & (c) by varying Nt and  $\delta$ 

respectively. Fig. 7(d) shows that  $\phi_t$  is oscillating nature for different values of t, and maximum near the top wall. Also, we can see that in these figures,  $\phi_t$  is wavering nature.

Table 2 shows the variations in the steady heat transfer rate (steady Nusselt number  $(Nu_s)$ ), unsteady heat transfer rate (unsteady Nusselt number  $(Nu_i)$ ), the steady mass transfer rate (steady Sherwood number  $(Sh_s)$ ), and unsteady mass transfer rate (unsteady



Fig. 6 — Steady nanoparticle concentration when Le = 0.5 (a) influence of  $\gamma = 1, 2, 3$ , (b) influence of Le = 0.1, 0.2, 0.3, (c) influence of Nt = 0.1, 0.2, 0.3, (d) influence of Nb = 0.1, 0.2, 0.3 and (e) influence of  $\delta = 0.1, 0.2, 0.3$ 





Fig. 7 — Unsteady nanoparticle concentration when H = 2.5 (a) influence of Nb = 0.1, 0.2, 0.3, (b) influence of Nt = 0.1, 0.2, 0.3, (c) influence of  $\delta = 0.1, 0.2, 0.3$ , and (d) influence of  $t = \pi, \frac{3\pi}{4}, \frac{2\pi}{3}, \frac{\pi}{2}, \frac{\pi}{3}, 2\pi$ 

Table 2 — Variations of steady Nusselt number  $Nu_s = (\theta_0'(y))$ , unsteady Nusselt number  $Nu_t = (\varepsilon \theta_1'(y)e^{it})$ , steady Sherwood number  $Sh_s = (\phi_0'(y))$ , and unsteady Sherwood number  $Sh_t = (\varepsilon \phi_1'(y)e^{it})$  at the wall y = 0 for various values of Ec, Nb, Nt, M, Rd,  $\delta$  when Pr = 21,  $K_1 = 0.001$ ,  $\gamma = 1$ ,  $\lambda_1 = 0.5$ ,  $\lambda_2 = 0.8$ ,  $\omega = 2$ ,  $t = \pi/3$ ,  $\varepsilon = 0.001$ 

Parameter	values	$Nu_s$	$Nu_t$	$Sh_s$	$Sh_t$
	0	0.000659	0.000627	-0.000733	-0.000059
Ec	0.5	0.700450	0.002367	-0.058586	-0.000428
	1	1.557516	0.004565	-0.139153	-0.001016
Nb	0.1	0.700364	0.002362	-0.116278	-0.000855
	0.2	0.700450	0.002367	-0.058586	-0.000428
	0.3	0.700507	0.002371	-0.039361	-0.000285
Nt	0.1	0.669287	0.002191	-0.027867	-0.000183
	0.2	0.700450	0.002367	-0.058586	-0.000428
	0.3	0.739908	0.002594	-0.093907	-0.000758
М	1	1.050273	0.003087	-0.092007	-0.000635
	2	0.700450	0.002367	-0.058586	-0.000428
	3	0.436252	0.001789	-0.035218	-0.000277
Rd	1	0.700450	0.002367	-0.058586	-0.000428
	2	0.621620	0.001672	-0.041757	-0.000229
	3	0.613134	0.001354	-0.029413	-0.000157
δ	0.1	0.700450	0.002367	-0.058586	-0.000428
	0.2	0.761188	0.003822	-0.067040	-0.000786
	0.3	0.844957	0.006659	-0.078440	-0.001761

Sherwood number  $(Sh_i)$  at the lower wall for various values of Ec, Nb, Nt, M, Rd, and  $\delta$ . One can be noted that both  $Nu_s$  and  $Nu_t$  are increased with the rise in Eckert number (Ec), Brownian motion parameter (Nb), thermophoresis parameter (Nt), and thermal relaxation time parameter  $(\delta)$ . Furthermore, it is observed that  $Nu_s$  and  $Nu_t$  are decreasing functions of Hartmann number (M), and radiation parameter (Rd). This table exhibition  $Sh_s$  and  $Sh_t$  are decreased for a given rise Nt, Ec and  $\delta$ . Furthermore, from

this table one can note that  $Sh_s$  and  $Sh_t$  are increasing functions of M, Nb, and Rd.

## **5** Conclusion

This study examines the pulsatile flow of Oldroyd-B nanofluid in a porous channel subjected to a chemical reaction, viscous dissipation, and Joule heating with the Cattaneo-Christov heat flux model. By using the perturbation approach, the PDEs are converted into ODEs and solved numerically using the Runge-Kutta fourth-order scheme using the shooting approach. The effects of relevant parameters have been analyzed on the flow variables. The most important results are as follows:

- The steady velocity increases with higher frequency parameter, and while it falls with rising Hartmann number, and cross-flow Reynolds number.
- The unsteady velocity of nanofluid enhances with a rise in λ<sub>1</sub>, H while it is reduced with a rise in M, λ<sub>2</sub>, R.
- There is an enhancement in  $\Theta_s$  of nanofluid for the higher values of Ec, Rd, Nb and Nt.
- $\theta_r$  distribution demonstrates wavering nature and the supreme is near the suction wall.
- The steady nanoparticle concentration distribution declines with a gain of Le,  $\gamma$ , Nb while it grows for a given rise in Nt and  $\delta$ .
- $Nu_s$  and  $Nu_t$  are increasing functions of Nb, Nt, Ec and  $\delta$ .
- $Sh_s$  and  $Sh_t$  are reducing functions of Nt,  $\delta$  and Ec while they are increasing functions of Nb, M, and Rd.

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